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Prediction of free air space in initial composting mixtures by a statistical design approach

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ABSTRACT

Free air space (FAS) is a physical parameter that can play an important role in composting processes to maintain favourable aerobic conditions. Aiming to predict the FAS of initial composting mixtures, specific materials proportions ranged from 0 to 1 were tested for a case study comprising industrial potato peel, which is characterized by low air void volume, thus requiring additional components for its composting.

The characterization and prediction of FAS for initial mixtures involving potato peel, grass clippings and rice husks (set A) or sawdust (set B) was accomplished by means of an augmented simplex-centroid mixture design approach. The experimental data were fitted to second order Scheffé polynomials. Synergistic or antagonistic effects of mixture proportions in the FAS response were identified from the surface and response trace plots in the FAS response. Moreover, a good agreement was achieved between the model predictions and supplementary experimental data. Moreover, theoretical and empirical approaches for estimating FAS available in literature were compared with the predictions generated by the mixture design approach.

This study demonstrated that the mixture design methodology can be a valuable tool to predict the initial FAS of composting mixtures, specifically in making adjustments to improve composting processes containing primarily potato peel.

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1. Introduction

Potato peel (PP) waste is a by-product from the processed potato products industries such as French fries, chips and puree. Although PP is a zero value waste for those plants, disposal, sanitation, and environmental problems must be overcome ([Arapoglou et al.,](#page-6-0) [2010\)](#page-6-0). During the processing of potatoes at industrial level, depending on the technology used (steam, abrasion or lye peeling) losses caused by potato peeling can reach 15-40% of the total raw materials [\(Schieber et al., 2001\)](#page-7-0).

Though the food industry manages PP waste as a non-valuable by-product, its composition may be suitable for several applications such as dietary fibre for baking products and animal feeding ([Djomo et al., 2008\)](#page-7-0), biohydrogen and ethanol production ([Arapoglou et al., 2010;](#page-6-0) [Djomo et al., 2008;](#page-7-0) [Mars et al., 2010](#page-7-0)), source of natural antioxidants ([Al-Weshahy et al., 2013;](#page-6-0) [Schieber et al.,](#page-7-0)

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[2001](#page-7-0); [Wijngaard et al., 2012](#page-7-0)) and bio-methane production ([Parawira et al., 2004](#page-7-0); [Kaparaju and Rintala, 2005;](#page-7-0) [Kryvoruchko](#page-7-0) [et al., 2009](#page-7-0)). Our study addressed the PP valorisation through composting. This process may be defined as the biological decomposition and stabilization of organic subtracts, under aerobic conditions that allow development of thermophilic temperatures, as result of biologically generated heat, to obtain a final product that is stable, free of pathogens and plant seeds, that can be beneficially applied to land ([Haug, 1993](#page-7-0)). It should be noted that PP valorisation by composting can be quite interesting for the food industry, given that a volume reduction of by-products up to 40% can be achieved ([Schaub and Leonard, 1996\)](#page-7-0). Nevertheless, to the best of our knowledge, PP composting has been scarcely addressed in literature. PP waste is usually characterized by high interparticle water content which might hinder composting evolution, due to higher oxygen diffusion resistance in pores between particles. Therefore, its valorization may require previous mixture with other materials, aiming to reach an adequate formulation for composting.

Mixture formulations for composting are often based on physical and chemical properties of the wastes [\(Barrena et al., 2011\)](#page-6-0) in

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order to adjust moisture content and C:N ratio to optimal values that favor growth and activity of microbial populations. Indeed, it is well known that one of the most important factors for thermophilic composting is the carbon to nitrogen ratio (C/N) with optimum values around 25-30:1 [\(Abdullah and Chin, 2010;](#page-6-0) [Hamoda et al.,](#page-7-0) [1998](#page-7-0); [Huang et al., 2006](#page-7-0)) and moisture content in the range of 50-65% ([Abdullah and Chin, 2010;](#page-6-0) [Liang et al., 2003\)](#page-7-0).

However, more recently the free air space (FAS) of a mixture has also been indicated as a physical property that may play an important role during composting [\(Agnew et al., 2003;](#page-6-0) [Barrena](#page-6-0) [et al., 2011;](#page-6-0) [Eftoda and McCartney, 2004;](#page-7-0) [Richard et al., 2004](#page-7-0); [Ruggieri et al., 2009\)](#page-7-0). This parameter is defined as the ratio of gas filled pore volume to total compost mixture volume and it determines the air quantity and movement inside the mixture, as well as the intrinsic air content, carbon dioxide, moisture and heat removal from the system [\(Richard et al., 2004](#page-7-0); [Ruggieri et al., 2009\)](#page-7-0). FAS depends on the structural characteristics of the materials used such as bulk density, particle density and water content. A minimum value of 30% is usually required to ensure aerobic condition in the composting mixture [\(Haug, 1993\)](#page-7-0), and optimum values for FAS may be in the range of 60%. In literature there are references to FAS as high as 85–90% without significant negative impact ([Ahn et al.,](#page-6-0) [2008](#page-6-0); [Ruggieri et al., 2009](#page-7-0)). To quantify FAS for a given composting mixture, some theoretical empirical correlations have been developed ([Agnew et al., 2003](#page-6-0); [Haug, 1993](#page-7-0), [Oppenheimer et al., 1997](#page-7-0); [Richard et al., 2004](#page-7-0)). Moreover, experimental procedures by using air pycnometry have been studied and compared ([Ruggieri et al.,](#page-7-0) [2009](#page-7-0)). But so far, the study of an approach able to predict FAS for a given mixture based on its individual components proportions has been seldom addressed ([Soares et al., 2012\)](#page-7-0).

Mixture design is a statistical technique associated to the concept of planning and execution of informative experiments concerning a mixture of different components, and it has been widely used to establish formulations in chemical, pharmaceutical and food industries ([Eriksson, 1998](#page-7-0)). The method consists in varying the proportions of two or more ingredients of the mixture and studying the influence of the independent variables (proportions of different components) into the measured response, which is dependent on the ingredient composition ([Akalin et al., 2010](#page-6-0)).

In this scope, our work aims to use the mixture design approach to understand and predict the influence of each component, on the FAS of an initial mixture containing primarily potato peel waste (PP) for further composting. Rice husk (RH) or sawdust (SD) were selected as bulking agents, and grass clippings (GC) as nitrogen source.

2. Materials and methods

2.1. Composting materials

The materials used were collected from different sources: potato peel (PP) is from a national industry of potato chips, rice husk (RH) was provided by a rice husking factory, sawdust (SD) is from a local pine sawmill, and grass clippings (GC) were obtained from a national football stadium. Grass clippings were sieved through a 5 cm mesh to obtain a homogeneous material in size and shape. The other materials did not require any specific treatment. The characterization of the each material was carried out using a composite sample of 25 L obtained from five individual samples of 5 L taken from the initial laboratory samples of about 120 L. Then, each composite sample of 25 L was homogenized and divided into four parts, with one being eliminated. This procedure was repeated until samples of about $1-2$ L were obtained for further analysis.

2.2. Mixture design establishment and validation

The mixtures tested in this study were grouped in two sets (Set A and Set B) according to the type of bulking agent used. Each set comprised three mixture factors or ingredients (set A: $PP + GC + RH$); (set B: $PP + GC + SD$) and their mixing proportions were individually allowed to range from 0 to 1.

Therefore, a regular and triangular experimental design region is expected for each set, with the constraint that the sum of all feedstock's proportions must be 1. Vertices of the design region correspond to the formulations that are pure blends.

The main objective of this design was to predict the free air space (desired response) for any mixture tested by modelling the mixing surface with mathematical equations. It was assumed that the measured response was only dependent on the relative proportions of the ingredients (considered as independent variables) but not on the amount of the mixture.

The models considered in this study were Scheffé canonical polynomials [\(Smith, 2005\)](#page-7-0):

 $E(Y)$

Linear:

Quadratic:

Special cubic:

$$
E(Y) = \sum_{i=1}^{q} \beta_i X_i + \sum_{i=1}^{q-1} \sum_{j=i+1}^{q} \beta_{ij} X_i X_j
$$

+
$$
\sum_{i=1}^{q-2} \sum_{j=i+1}^{q-1} \sum_{k=j+1}^{q} \beta_{ijk} X_i X_j X_k
$$
(3)

 $E(Y) = \sum_{i=1}^{q} \beta_i X_i$ (1)

 $i = 1$ $\frac{q}{\sum}$

 $\sum_{j=i+1} \beta_{ij} X_i X_j$ (2)

 $E(Y) = \sum_{i=1}^{q} \beta_i X_i + \sum_{i=1}^{q-1}$

Full cubic:

$$
= \sum_{i=1}^{q} \beta_{i}X_{i} + \sum_{i=1}^{q-1} \sum_{j=i+1}^{q} \beta_{ij}X_{i}X_{j}
$$

+
$$
\sum_{i=1}^{q-1} \sum_{j=i+1}^{q} \gamma_{ij}X_{i}X_{j}(X_{i}-X_{j})
$$
 (4)
+
$$
\sum_{i=1}^{q-2} \sum_{j=i+1}^{q-1} \sum_{k=j+1}^{q} \beta_{ijk}X_{i}X_{j}X_{k}
$$

Special Quartic:

$$
E(Y) = \sum_{i=1}^{q} \beta_{i} X_{i} + \sum_{i=1}^{q-1} \sum_{j=i+1}^{q} \beta_{ij} X_{i} X_{j}
$$

+
$$
\sum_{i=1}^{q-1} \sum_{j=i+1}^{q} \gamma_{ij} X_{i} X_{j} (X_{i} - X_{j})
$$

+
$$
\sum_{i=1}^{q-2} \sum_{j=i+1}^{q-1} \sum_{k=j+1}^{q} \beta_{ijk} X_{i}^{2} X_{j} X_{k}
$$

+
$$
\sum_{i=1}^{q-2} \sum_{j=i+1}^{q-1} \sum_{k=j+1}^{q} \beta_{ijk} X_{i} X_{j}^{2} X_{k}
$$

+
$$
\sum_{i=1}^{q-2} \sum_{j=i+1}^{q-1} \sum_{k=j+1}^{q} \beta_{ijk} X_{i} X_{j} X_{k}^{2}
$$

where $E(Y)$ is the expected value of the output variable Y, X are the independent variables, β and γ correspond to the polynomial coefficients, q is the number of components (in this case $q = 3$).

Since the experimental mixture region is regular and constitutes a simplex shaped region, an augmented simplex-centroid mixture design approach was used to define the number of mixtures necessary to attain the desired response (FAS value). This

Fig. 1. Mixtures tested according to a simplex-centroid mixture design (values in brackets represent mixture order preparation and analysis).

approach allows to detect the model curvature in the interior of the design region and it includes the points (mixtures) indicated in Fig. 1, namely pure mixtures (vertices of the triangle), binary mixtures (midpoints at each side of the triangle), and mixtures involving three components. In the interior area of the triangle there is a mixture of one third each of all ingredients (called centroid point) and three mixtures located midway between the centroid and each pure material. The pure and centroid mixtures were analysed twice to detect possible lack of fit and pure experimental error. According to this methodology, each set comprised 14 experiments.

Each mix was prepared, for a total load of 2 kg, by weighing the different components and mixing them by hand during 10 min, according to the pre-defined proportions and random sequential order indicated in Fig. 1. Before mixture preparation, every single individual ingredient was manually mixed to promote homogenisation prior to weighing. Design-Expert \mathcal{P} version 8.0.4 was used to analyse experimental data and to evaluate of the model that best fits the composition effects in the response variables.

Some extra mixtures were prepared and analysed to validate the response of the model. This assessment was accomplished by comparing the model predictions and experimental FAS values for these specific mixtures.

2.3. Analytical methods

The main response variable under analysis is FAS and was calculated according to Eq. (6) ([Adhikari et al., 2009](#page-6-0)):

$$
\text{FAS} = \left(1 - \frac{\text{BD}}{\text{PD}}\right) \times 100\% \tag{6}
$$

where BD is the wet bulk density ($kg \, \text{m}^{-3}$) and PD is the wet particle density of the mixture (kg m^{-3}).

The parameter BD was determined according to a standard procedure described elsewhere [\(US Department of Agriculture and](#page-7-0) [US Composting Council, 2001](#page-7-0)), and PD was estimated based on the procedure defined by [Adhikari et al. \(2009\)](#page-6-0). Water absorption capacity (WAC) of the bulking agents tested was performed as described by [Adhikari et al. \(2008\).](#page-6-0)

Moisture content of each fresh sample was determined by drying it in an oven at 105 \degree C until constant weight. Organic matter was measured as volatile solids (VS) by burning 2.5 g dry sample in a muffle furnace at 550 °C for 4 h (until constant weight). Total organic carbon (C_{org}) was determined in a Carbon-Sulphur Analyzer (Leco Instruments, model SC-144 DR), where carbon was oxidized to carbon dioxide by heating at 550 \degree C. The total nitrogen content (N) was quantified by elemental analysis (EA 1108 CHNS-O-Fisons). All determinations were performed at least in triplicate.

3. Results and discussion

3.1. Characterization of the composting materials

Physical and chemical parameters determined for the individual materials are shown in Table 1, where the results were reported by mean \pm standard deviation and the values in brackets indicate the number of samples analysed.

These determinations show that the key component under analysis, PP, is characterized by the highest moisture content and the lowest FAS. Indeed, although PP revealed a favourable C_{ore}/N ratio for microbial activity, its valorisation throughout composting may be hindered by the low inter-particle volume of voids available for oxygen diffusion.

With respect to rice husks and sawdust both have been extensively used in composting as structural or drying amendments to reduce bulk density and increase air voids of the mixture ([Chang](#page-6-0) [et al., 1999](#page-6-0); [Chang and Hsu, 2008](#page-6-0); [Gao et al., 2010;](#page-7-0) [Huang et al.,](#page-7-0) [2006;](#page-7-0) [Jolanun et al., 2008](#page-7-0); [Nakasaki et al., 1986,](#page-7-0) [1989\)](#page-7-0). In our

Table 1

Physical and chemical properties of individual mixture components.

Abbreviations: MC-moisture content; VS-volatile solids; BD-wet bulk density; FAS-free air space, C_{org}-organic carbon; WAC-Water absorption capacity; n.d.-not determined.
^a Calculated by using Eq. (6).

^b All particles with dimensions less than 2 cm.

study, these materials exhibited low moisture content (less than 12%) and high water absorption capacity (440% for SD and 350% for RH) which are compatible to the purpose of correcting moisture excess of PP. In addition, the high FAS of these components (about 80%) indicates that they are able to maintain air spaces between particles in the composting mixture with PP waste and ensure its proper aeration. With respect to GC, this material also exhibits high FAS. However, in this case it decomposes rapidly during composting, and thus it is not a good bulking agent for composting mixtures. On the other hand, its low C_{org}/N ratio turns GC into a good nitrogen source whenever necessary. In summary, the ingredients selected in this study seem to be adequate to obtain well balanced mixtures, since their properties are complementary.

3.2. Response regression model analysis

To evaluate how a specific composition determines the FAS for mixtures containing PP, GC and RH or SD as bulking agents, experimental responses of FAS were obtained for each trial listed in Table 2. Those responses were fitted to Eqs. [\(1\) to \(3\)](#page-1-0) by using Design-Expert $^{\circledast}$. Full cubic, Eq. [\(4\)](#page-1-0), and special quartic, Eq. [\(5\),](#page-1-0) models were excluded from the evaluation, because the number of model terms should be less than to the number of unique points in the design (10 in our experimental design).

The polynomial fitting results are presented in Table 3 with respect to common statistical parameters, lack of fit and sequential model sum of squares. In fact, the model summary statistics includes standard deviation, R_{adj}^2 (proportional reduction in the variance resulting from fitting the model), R_{pred}^2 (amount of variation in new data explained by the model) and PRESS statistic (residual error sum of squares, which describes how well the model fits data).

The lack of fit compares the residual error with the error expected in the response, if the experiment is repeated (pure error). Since it is not desirable that residual error significantly exceeds the pure error, models with a p-value greater than 0.1 should be considered. Regarding sequential model sum of squares, this parameter represents the sum of the squared deviations from the mean for each model, and it indicates the overall cumulative improvement in the fit as terms are added.

Among the regression models under consideration, the selection of the best one to predict the experimental response was based on the following criteria: i) Low standard deviation, high R_{adj}^2 and R_{pred}^2 and low PRESS; ii) Low probability of response improvement as additional terms are added (p-value in the sequential model sum of squares less than 0.05); iii) High p-value in the lack of fit test.

Therefore, for set A, special cubic model complies with criteria i) and iii); however, the *p-value* associated to the sequential model sum of squares indicates that there is no significant improvement of the model fit due to additional terms. Hence, a quadratic model was selected in this case. For set B, criteria i) and iii) were fulfilled by quadratic and special cubic models. Nevertheless, the probability of response improvement was low for the higher order model, and thus the quadratic model was also selected.

The regression coefficients obtained for the selected models are shown in [Table 4.](#page-4-0) The second order polynomial describing FAS response for mixtures with PP:GC:RH presented a non-linear term (X_2X_3) that is not significant. Therefore, a reduced model was evaluated, by removing the term with the highest p-value until all p-values are less than 0.1 [\(Smith, 2005\)](#page-7-0). This procedure was performed using Design-Expert $^{\circledR}$ and led to the response indicated in [Table 4](#page-4-0). As a result, parameters R_{adj}^2 and R_{pred}^2 were slightly improved (from 0.995 to 0.996 and 0.985 to 0.991, respectively).

Set A			Set A (reduced model)		Set B		
Coefficient value	Independent variable	Term <i>p-value</i> ^a	Coefficient value	Independent variable	Coefficient value	Independent variable	Term <i>p-value^a</i>
34.56	Λ.		34.52	A۰	24.79	A1	
86.40	X_2		86.61	X_2	85.74	X_2	
86.77	X_3		86.97	X_3	84.13	X_3	
50.41	X_1X_2	< 0.0001	50.81	X_1X_2	61.55	X_1X_2	< 0.0001
92.98	X_1X_3	< 0.0001	93.38	X_1X_3	68.66	X_1X_3	< 0.0001
3.24	X_2X_3	0.5351		X_2X_3	-38.85	X_2X_3	0.0002

Regression coefficients of the quadratic model for predicting FAS of set A (with RH) and B (with SD).

^a If a term is not significant for the model, then p-value is > 0.05 and model reduction should be evaluated.

As usual, obtained models for predicting FAS were based on the assumption that errors are independent and identically distributed with zero mean and homogeneous variance [\(Smith, 2005\)](#page-7-0). The confirmation of these conditions was performed by visual inspection of the normal probability plot of the studentized residuals (to check for normality of residuals), by comparing their values with the predicted ones (data not shown). Although it was observed some scatter, normal plot of residuals followed a straight line suggesting a normal distribution.

3.3. Surface and response trace plots analysis

Table 4

Trace and surface/contour plots were drawn to evaluate the effects of individual ingredients on FAS response. For sets A and B, surface plots are depicted in Fig. 2a-b, which include the projection of the response in a 2D representation. In these figures, mixture compositions that produced the same response are indicated by a contour line. For both sets A and B, maximum FAS values are located towards pure blends of GC and RH/SD. In fact, contour lines in Fig. 2a-b indicate a broad range of GC and RH/SD proportions where FAS assume identical values. It should be noted that large amounts of GC may seem to ensure high values for FAS. However, this material decomposes quickly and then tend to compact, reducing pores between compost particles ([Rynk et al., 1992\)](#page-7-0). Moreover, the response surface in Fig. 2-b shows that the binary mixture of SD with GC acts antagonistically on FAS parameter, which is reflected in the negative coefficient associated to X_2X_3 (Table 4).

The main reason for this result is the great importance of the particle size distribution of the bulking agent to the structural condition of the mixture. In our study, 86% of SD particles are lower than 2 mm, which is a high value comparing with the one suggested by [Haug \(1993\)](#page-7-0) (50% of particles passing a mesh of 2.23 mm). By mixing SD with GC, the interstices of GC were probably occupied by sawdust, thus reducing FAS, rather than what is expected of a good bulking agent.

Trace plots, Fig. 2 $c-d$, enable to compare the effects of all components in the design space and determine the sensitivity of the response to deviations from the formulation near the reference mixture (the centroid of the triangle, design points n° 9 and 14 from

Fig. 2. Contour plots for FAS: a)- set A (A:PP; B: GC; C: RH); b)- set B (A:PP; B: GC; C: SD); response trace plots for FAS: c)- set A; d)- set B.

[Table 1](#page-2-0)). The lines in [Fig. 2](#page-4-0) c-d correspond to the FAS response due to variations in the proportions of a selected component, keeping constant the ratio of the others ingredients and the sum of mixture components equal to one. The results reveal that independently of the bulking agent used, PP (ingredient A) has a strong effect on the reduction of FAS as mixtures deviate from the centroid. When RH is used, [Fig. 2-](#page-4-0)c, the response trace to GC is nearly a horizontal line, meaning that it has a negligible effect on FAS. When SD is tested, [Fig. 2-](#page-4-0)d, GC and SD response curves are overlapped, and thus these components have roughly identical linear effect on FAS. This result may be explained by the particle size of the SD used in our study, as previously mentioned.

3.4. Validation of the response regression model

Three compositions were selected for each bulking agent, for validating regression models, Eqs (7) and (8), previously obtained for FAS:

$$
FAS_{Set A} = 34.52X_1 + 86.61X_2 + 86.97X_3 + 50.81X_1X_2
$$

+ 93.38X₁X₃ (7)

$$
FAS_{Set B} = 24.79X_1 + 85.74X_2 + 84.13X_3 + 61.55X_1X_2
$$

+ 68.66X₁X₃ - 38.85X₂X₃ (8)

The selection was based on the range of ingredients proportions that are favourable to composting in what concerns MC, C_{org}/N and FAS. Restrictions imposed to C_{org}/N are in the interval $20-40:1$ ([Rynk et al., 1992](#page-7-0)). The upper limit was slightly broadened for MC $(55-75%)$ due to the high absorption capacity of bulking agents involved [\(Barrena et al., 2011](#page-6-0)). Mixture proportions that fulfilled the requirements for MC and C_{org}/N were calculated according to the principle of mass conservation to a blend of PP, GC and RH or SD, whose characteristics were listed in [Table 1.](#page-2-0) FAS was allowed to vary between 60 and 85%. By combining the constraints of the parameters MC, C_{org}/N and FAS, an interception area (shaded region in Fig. 3) is defined for selecting the mixtures RH1 to RH3 and SD1 to SD3, for FAS model validation. The numerical results for validating the models described by Eq. (7) and Eq (8) are shown in [Table 5](#page-6-0). Experimental results for FAS were found to be very close to

the predictions of the models, with relative errors ranging from $-2.7-5.8$ %, but within the prediction intervals. Therefore, the models developed by mixture design approach for predicting FAS, Eqs. (7) and (8), can be used to properly calculate the free air space of ternary mixtures of PP, GC, RH or SD.

In this study FAS was quantified by using the simplest theoretical correlation available, Eq. [\(6\)](#page-2-0), although air pycnometry is pointed out as the most reliable technique for its determination in composting matrices ([Ruggieri et al., 2009\)](#page-7-0). But the unavailability of commercial pycnometers for this type of solid material, conditioned the cross-confirmation of our theoretical correlation based results.

In literature, FAS has been estimated by theoretical or empirical approaches ([Alburquerque et al., 2008](#page-6-0)). [Fig. 4](#page-6-0) compares FAS predictions of the models developed in our study, Eqs. (7) and (8), with the ones calculated by equations proposed by [Richard et al. \(2004\),](#page-7-0) Eq. (9), and [Agnew et al. \(2003\)](#page-6-0), Eq. (10):

$$
FAS_R = \left(1 - BD \times \left(\frac{1 - DM}{D_W} + \frac{DM \times OM}{PD_{OM}} + \frac{DM \times (1 - OM)}{PD_{ash}}\right)\right)
$$

× 100% (9)

$$
FAS_{Ag} = 100 - 0.0889 \times BD
$$
 (10)

where BD is the wet bulk density (kg m^{-3}), DM the fraction of dry matter, OM the fraction of organic matter in dry basis, D_w the density of water (kg m⁻³), PD_{OM} the particle density of organic matter (2500 kg m^{-3}) and PD_{ash} the particle density of ash $(1600 \text{ kg m}^{-3}).$

In general, for mixtures RH1 to RH3, FAS calculated by Eqs. (9) and (10) are slightly higher than the predicted by models of our study, Eqs. (7) and (8). However, in the case of SD1 to SD3 (sawdust as bulking agent), correlations values fitted inside the prediction intervals. These differences might be related to the applicability conditions of theoretical and empirical approaches for FAS quantification. According to [Ruggieri et al. \(2009\),](#page-7-0) properties such as BD and MC have a strong influence on FAS estimated by these correlations, and boundaries were established to its application. Namely,

Fig. 3. Contour and response trace plots for FAS for: a) set A (A:PP; B: GC; C: RH), RH1-RH3 are the validating mixtures; b) set B (A:PP; B: GC; C: SD), SD1-SD3 are the validating mixtures.

Table 5 Experimental conditions tested and validation results.

Mixt. ref.	X_1 (PP)	X_2 (GC)	X_3 (RH or SD)	MC(%)	VS $(%)$	BD (kg m^{-3})	FAS (%)		
							Exp. result	Model prediction	Pred. interval
RH ₁	0.587	0.192	0.219	70.5	86.7	240	75.8	73.9	± 4.2
RH ₂	0.506	0.324	0.170	69.6	85.9	229	76.4	76.7	± 4.0
RH ₃	0.660	0.081	0.259	64.3	86.2	245	73.9	71.0	± 4.5
SD ₁	0.400	0.400	0.200	67.5	90.5	325	71.3	73.3	± 5.3
SD ₂	0.343	0.516	0.141	71.4	88.5	268	78.3	76.0	± 5.3
SD3	0.600	0.300	0.100	70.8	90.0	440	66.9	63.0	± 6.5

Fig. 4. Comparison between FAS predictions error bars indicate prediction intervals with a significance of 95%.

 FAS_R , Eq. [\(9\),](#page-5-0) is limited for materials where BD is superior to 400 kg m $^{-3}$; below this level FAS_R may lead to misleading values. Also FAS_{Ag}, Eq. [\(10\),](#page-5-0) seems restricted only to high-moisture and/or low-density materials where FAS_R may provide misleading values. In our study, mixtures with RH have low bulk densities (<245 kg m $^{-3}$) and FAS_R were the highest ones, over estimating FAS_{model} (relative error ranged from –5.7 to –13.3%). FAS indicated by FAS_{Ag} were also overestimated but within the relative errors $(-3.8 \text{ to } -10.1\%)$. For mixtures with SD, FAS_R were more consistent with FAS_{model} predictions, especially for mixtures with higher bulk density (SD1 and SD3).

4. Conclusions

This study aimed to predict free air space of mixtures for further used in composting, based on mixture design approach. The organic materials tested were potato peel (PP), grass clippings (GC) and rice husks (RH) or sawdust (SD). The results proved that the mixture design methodology led to reliable mathematical models for predicting FAS of mixtures containing primarily PP. In particular, for mixtures with PP, GC and SD the FAS model pointed out the antagonistic effect of the binary mixture of GC and SD to the overall property. Contour plots revealed the occurrence of a wide range of GC and SD (bulking agent) proportions where FAS assume identical values; nonetheless, large proportions of GC should be avoided.

As expected, response trace plots clearly indicated that independently of the bulking agent used, the addition of potato peel has a strong effect on reducing the mixture air voids volume.

The models obtained for predicting FAS were compared with theoretical and empirical correlations proposed in literature which consider mixture properties like DM, OM and BD. For formulations with SD, correlations are consistent with our model prediction. When RH was used as bulking agent both literature correlations overestimated the FAS but even so the deviations were low.

In summary, mixture design approach led to good results to estimate FAS of initial mixtures with industrial potato peel waste, avoiding, this way, trial and error methods often used to establish the ingredients proportions. By overlapping contour plots that describe the influence of the mixture composition in FAS, it was possible to find a range that complies with requirements in what concerns moisture content, C/N ratio and FAS.

Future studies should address how model predictions are affected by two aspects: 1) variability of wet basis properties since they affect the surface areas of the feedstock particles and pore space formation and 2) biodegradability of the mixture, because when the materials decompose quickly, pores between particles are reduced and composting evolution may be hindered.

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